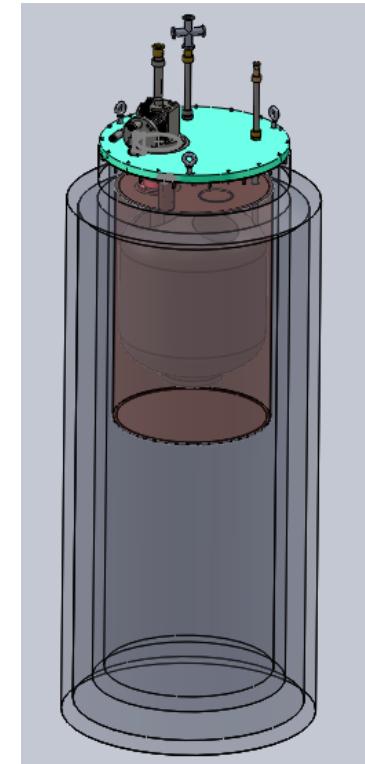


Thermal Analysis of Recondensing Systems

Professor John Pfotenhauer
(work performed by student Dan Schick)

Department of Mechanical Engineering
University of Wisconsin - Madison



Overview

- Goals
- Background
- Modeling
- Experimental Work
- Future Work

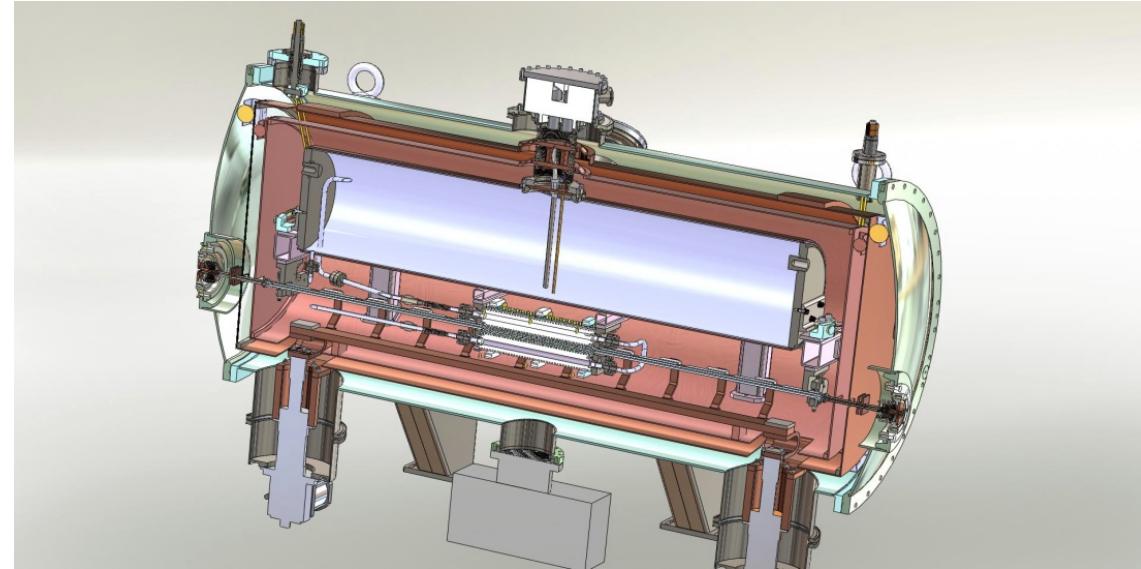


Image: Ivanyushenkov, Y. SCU0 Conceptual Design Review. 5 Feb 2010.

Goals

- Provide recommendations regarding liquid helium re-condensation
 - Develop models to estimate the thermal behavior of the re-condensing system
 - Film condensation
 - Vapor convection
 - Vessel conduction
 - Build and test different geometries
 - Baseline test
 - Surface enhancements

Length = 146 cm
Diameter = 30 cm

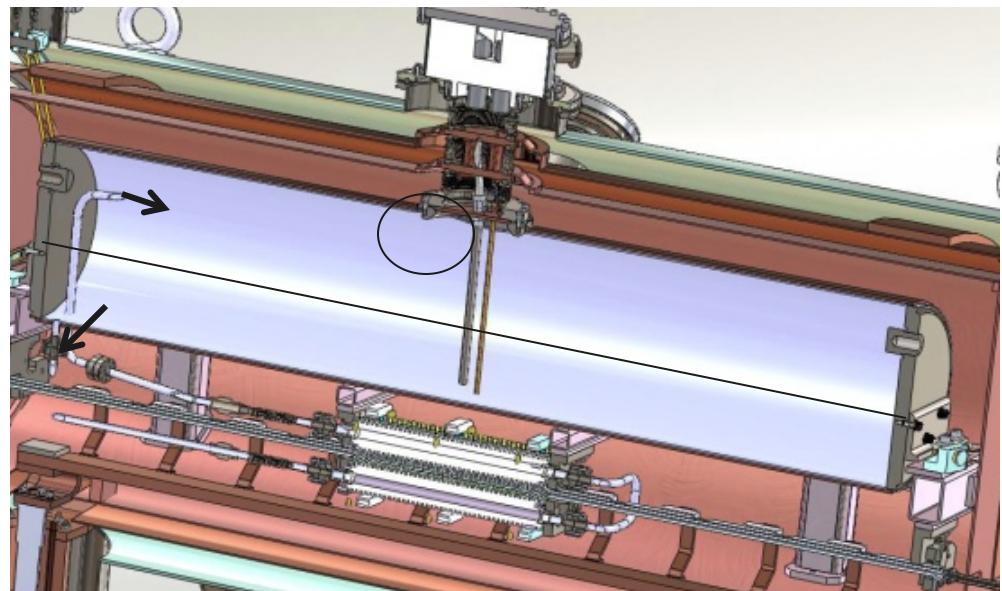
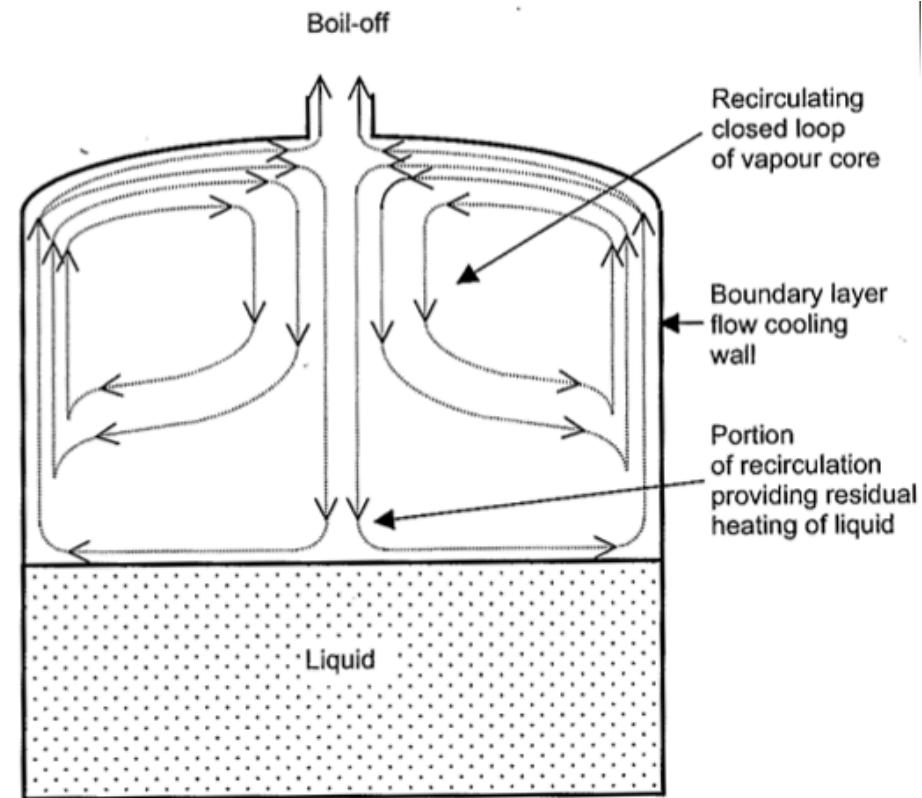


Image: Ivanyushenkov, Y. SCUO Conceptual Design Review. 5 Feb 2010.

Background

- University of Southampton
(Scurlock, ... 1978 - 2008)
 - Convective flows in stratified cryogen vapors
 - Upward convection along side walls, downward flow in the core
 - Conductive heat leak down dewar neck is reduced



Background

- Cryomech (Wang '05-'08):
 - LHe storage dewar at South Pole
 - 14 L/day ZBO
 - 2.7 L/day liquefaction
 - Improvements to liquefaction efficiency (w/ Scurlock)
 - Remove G10 sleeve, MLI, precooling heat exchanger
 - Add horizontal fins to OD of 2nd stage regenerator / pulse tube, and radiation shield to OD of 1st stage
 - Improve liquefaction from 12.8 L/day to 21.4 L/day

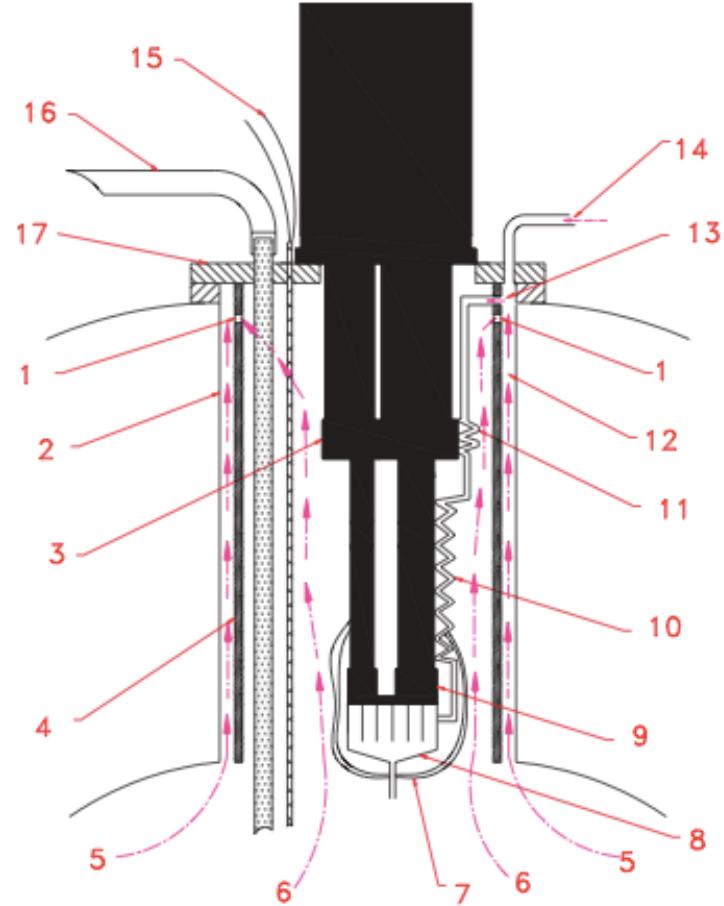
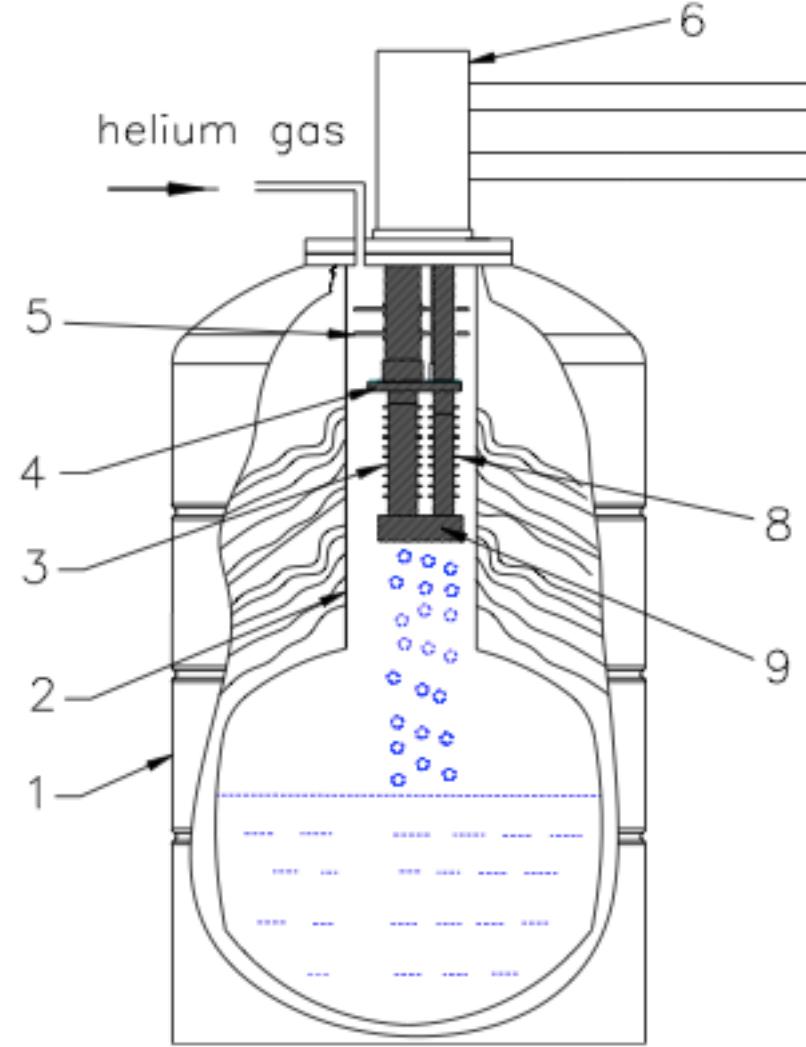


Fig. 2. Details of the pulse tube recondenser in the dewar: 1. holes for vapor flow of inside of G-10 sleeve; 2. dewar neck; 3. 1st stage heat exchanger of the cold head; 4. G-10 sleeve; 5. vapor in the circular gap; 6. vapor inside of G-10 sleeve; 7. superinsulation; 8. condenser; 9. 2nd stage heat exchanger of the cold head; 10. precooling heat exchanger on the 2nd stage regenerator; 11. precooling heat exchanger on the 1st stage; 12. annular flow channel; 13. gas inlet for liquefaction; 14. helium gas from outside of the dewar; 15. liquid level sensor; 16. liquid helium withdrawal line; 17. top flange.

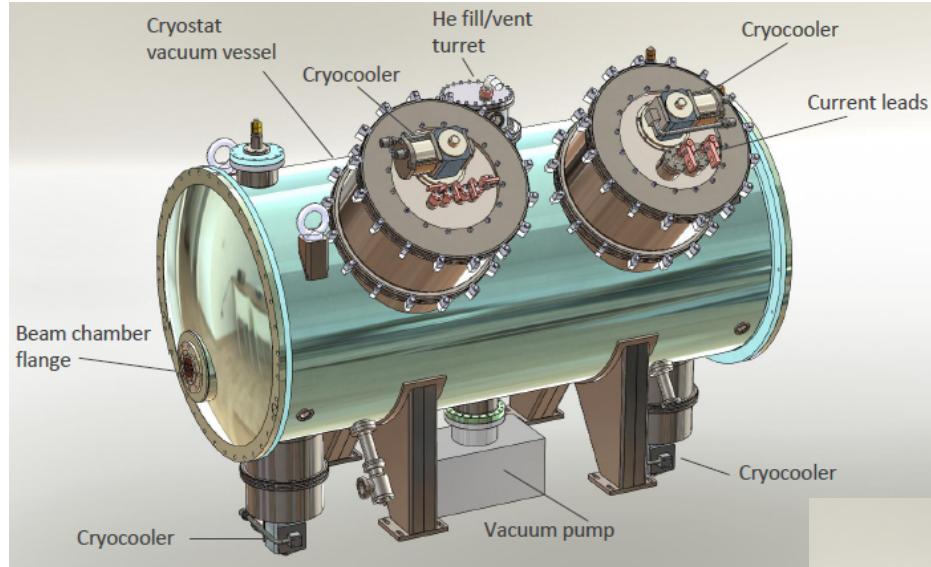
Background

- Cryomech (Wang '05-'08):
Re-condensers & Liquefiers
 - LHe storage dewar at South Pole
 - 14 L/day ZBO
 - 2.7 L/day liquefaction
 - Improvements to liquefaction efficiency (w/ Scurlock)
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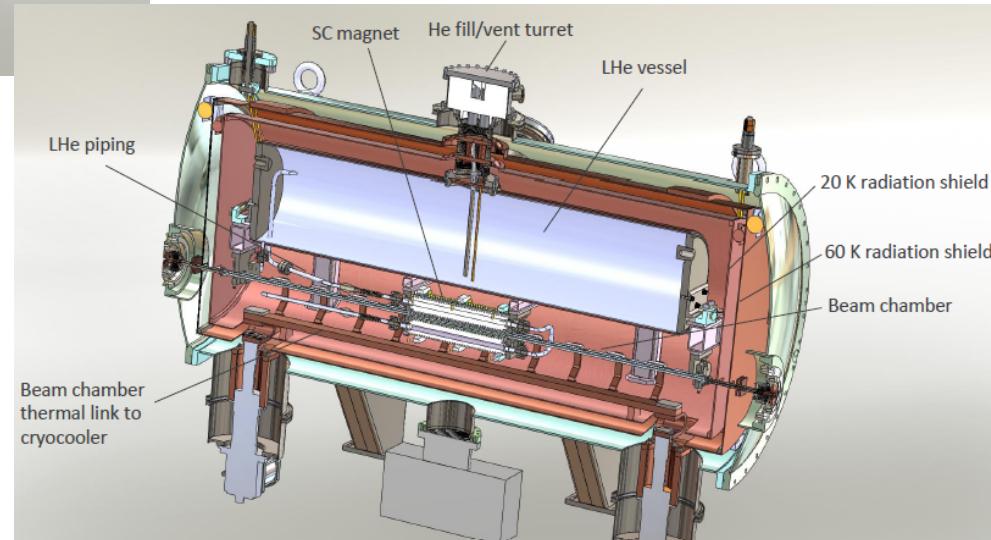
1. LHe dewar, 2. dewar neck, 3. fins on 2nd stage regenerator, 4. 1st stage, 5. radiation shields on 1st stage regenerator, 6. cryocooler valve head, 8. fins on 2nd stage pulse tube, 9. 2nd stage.

Superconducting Undulator Aparatus



Y. Ivanyushenkov, SCU0 Conceptual design review, February 5, 2010

1. GM cryocoolers mounted at angle (not vertical)
2. Only the bottom side of the 2nd stage is exposed to the helium vapor
3. Entire helium vapor region is maintained near 4 K

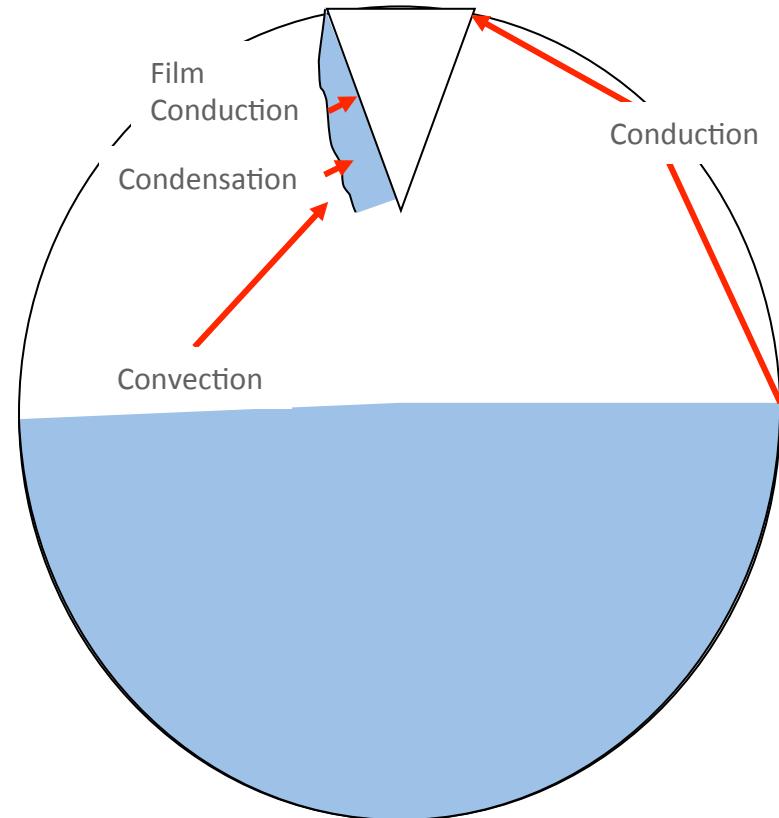
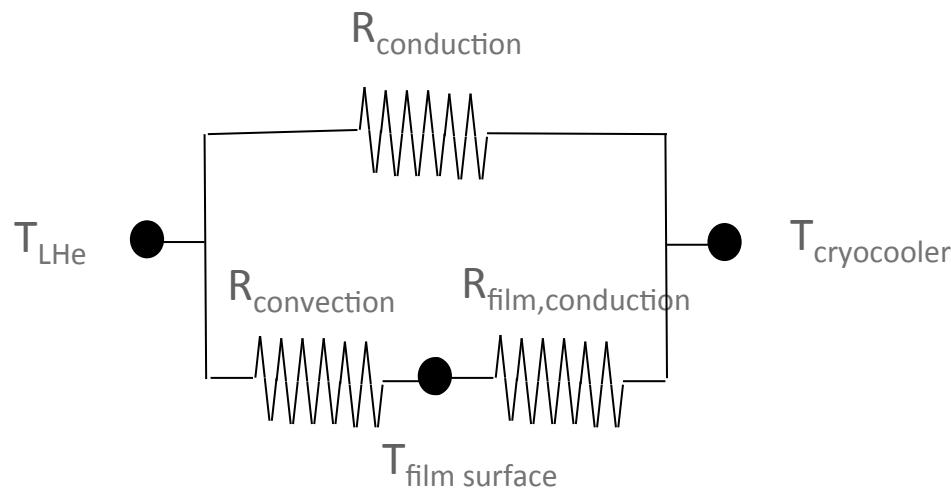


Y. Ivanyushenkov, SCU0 Conceptual design review, February 5, 2010

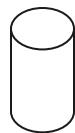
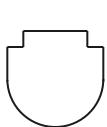
Thermal Modeling

Thermal Resistance Description

- Heat transfer in system represented by the resistance network shown (most basic terms)
 - Condensation & film conduction (EES)
 - Convection (ANSYS)
 - Conduction (FEHT)



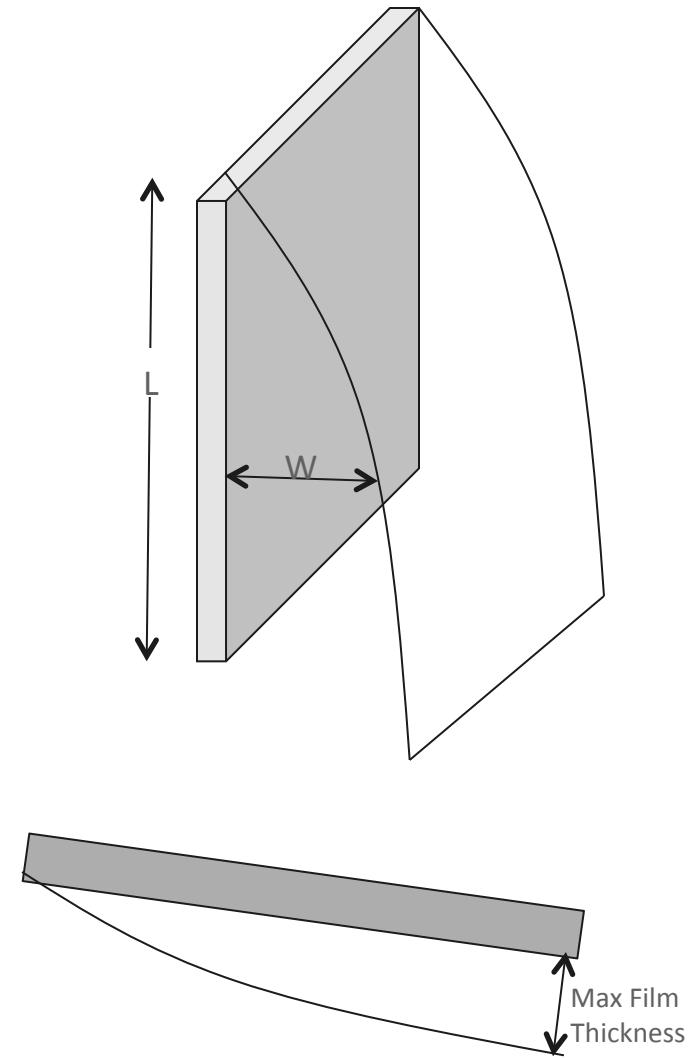
Condensation Considerations



- Film development on various geometries
- Maximum film thickness of helium
 - $\delta_{\max} = 0.3215 \text{ [mm]}$
 - 1 [atm], 4.2 [K], 0° from horizontal
 - $\delta_{\max} = 0.3317 \text{ [mm]}$
 - 1 [atm], 4.2 [K], 20° from horizontal

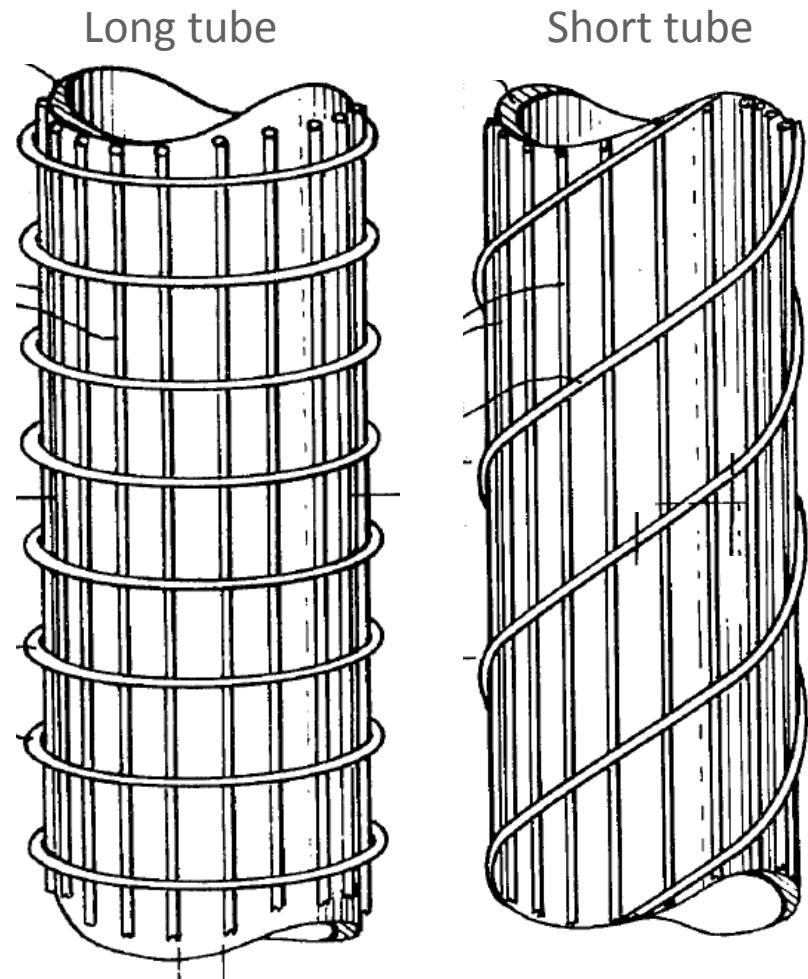
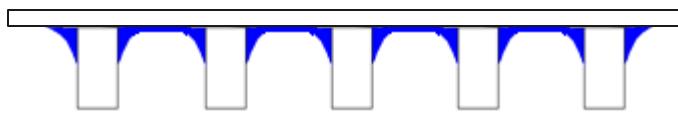
$$\delta_{\max} = \sqrt{\frac{\sigma_l}{g \cos(\theta) (\rho_l - \rho_v)}}$$

- Thin film = better heat transfer



Condensation Surface Enhancements¹

- Collect condensate into rivulets (streams)
- Thin film regions promote good heat transfer
- Surface tension used to concentrate the condensate into drainage rivulets
- Gravity also used to collect flow



1 Enhancement for Film Condensation Apparatus. Leslie C. Kun & Elias G. Ragi. United States Patent 4,253,519. March 3rd, 1981.

Thermal Resistance - Film Conduction/Condensation

- Heat of conduction

$$Q = \frac{k A}{\Delta L} \Delta T = \frac{1}{R} \Delta T$$

- Thermal resistance of conduction in parallel

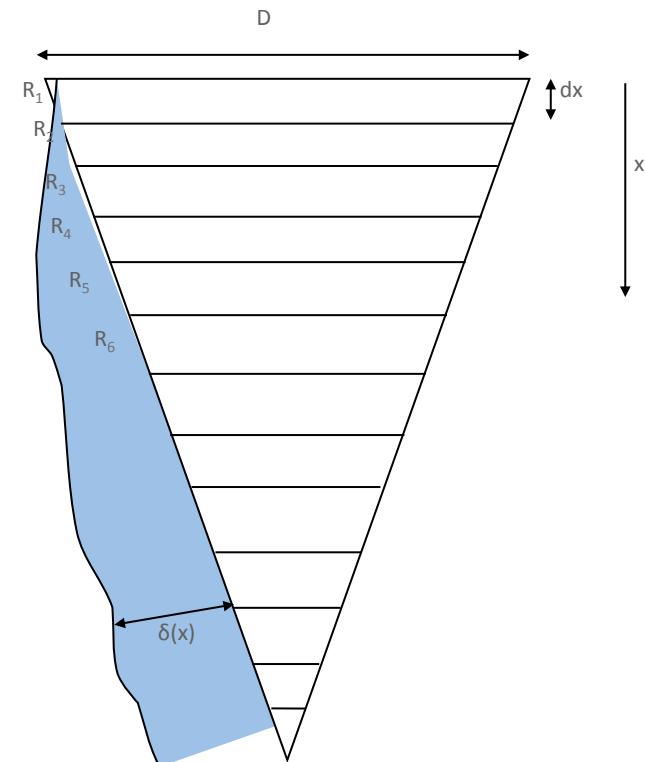
$$\dot{C}_{net} = \frac{1}{R_{net}} = \frac{k A(x_1)}{\Delta \delta(x_1)} + \frac{k A(x_2)}{\Delta \delta(x_2)} + \frac{k A(x_3)}{\Delta \delta(x_3)} + \dots$$

- Integrated thermal resistance as a function of height with changing geometry areas & film thicknesses

$$\dot{C}_{net} = \int \left(\frac{1}{R_{net}} \right) = \int_{x=0}^{x=L} \left(\frac{k P(x)}{\Delta \delta(x)} \right) dx$$

- Film condensation thickness

$$\delta = \left\{ \frac{4 x k_{l,sat} \mu_{l,sat} (T_{sat} - T_s)}{\rho_{l,sat} g \cos \theta (\rho_{l,sat} - \rho_{v,sat}) \left[\Delta i_{vap} + \frac{3 c_{l,sat} (T_{sat} - T_s)}{8} \right]} \right\}^{1/4}$$



δ = film thickness

$k_{l,sat}, \mu_{l,sat}, \rho_{l,sat}, \rho_{v,sat}, c_{l,sat}, \Delta i_{vap}$ = fluid properties

x = length of condensation surface

T_{sat} = Saturation temperature

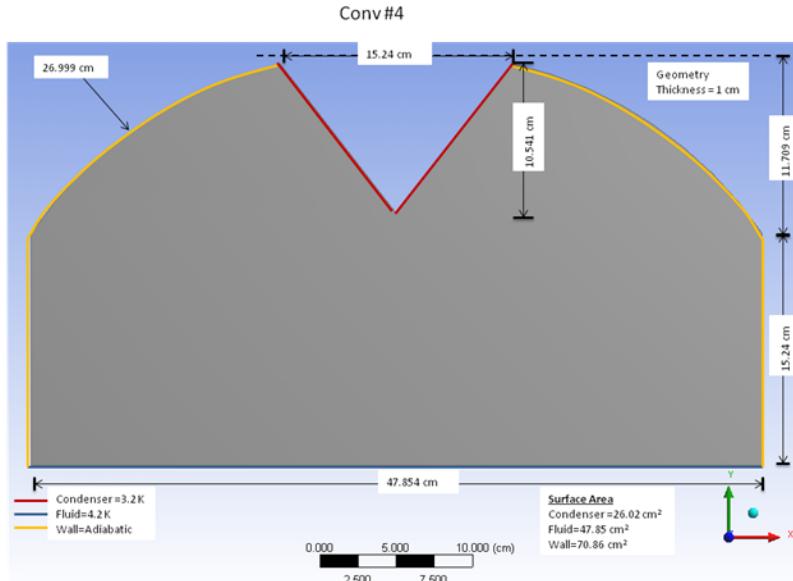
T_s = Surface temperature

g = gravitational acceleration

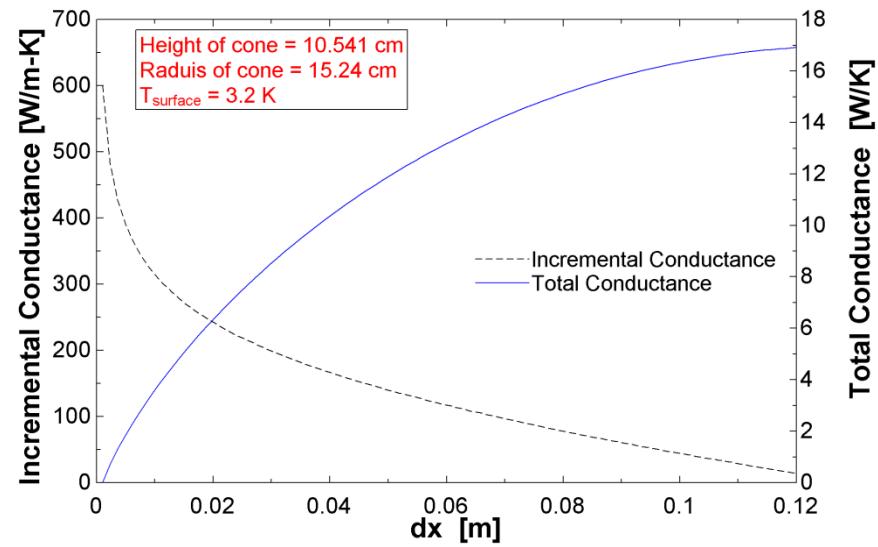
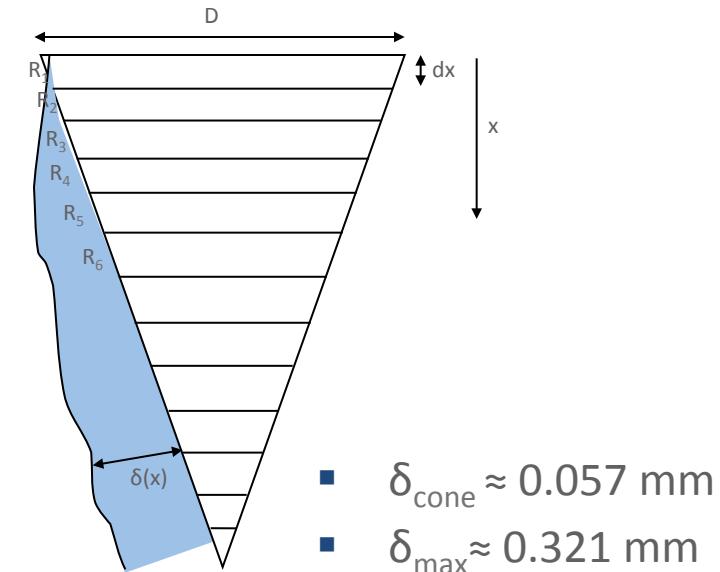
θ = angle of surface



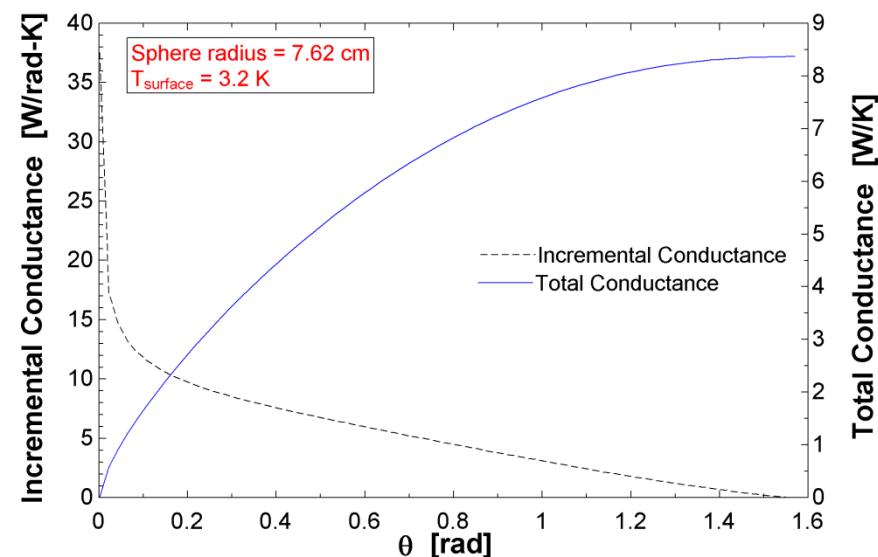
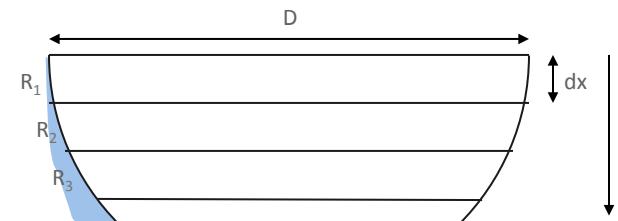
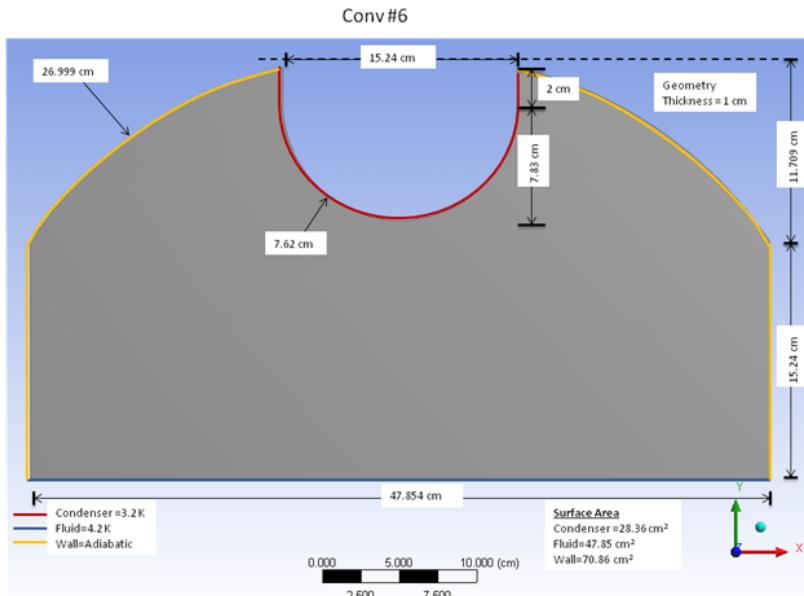
Thermal Resistance - Film Conduction (Cone)



- $R_{\text{conv}} \approx 20 \text{ K/W}$ (Dominant)
- $R_{\text{film,cond}} \approx 0.06 \text{ K/W}$



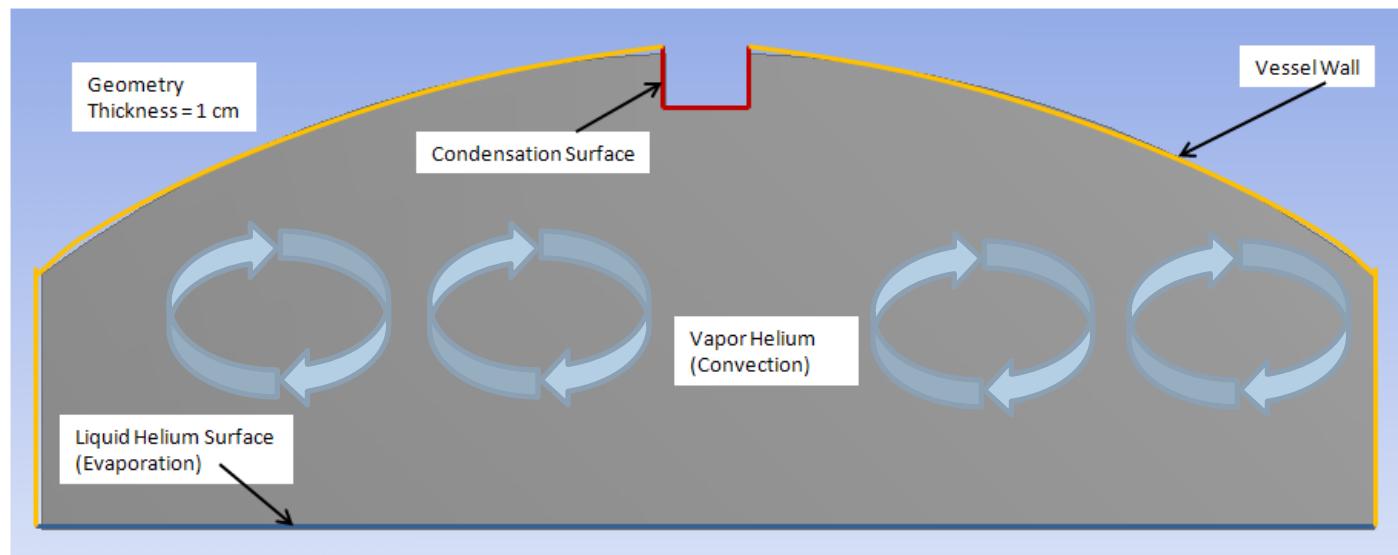
Thermal Resistance - Film Conduction (Hemisphere)



- $R_{conv} \approx 17 \text{ K/W}$ (Dominant)
- $R_{film,cond} \approx 0.12 \text{ K/W}$

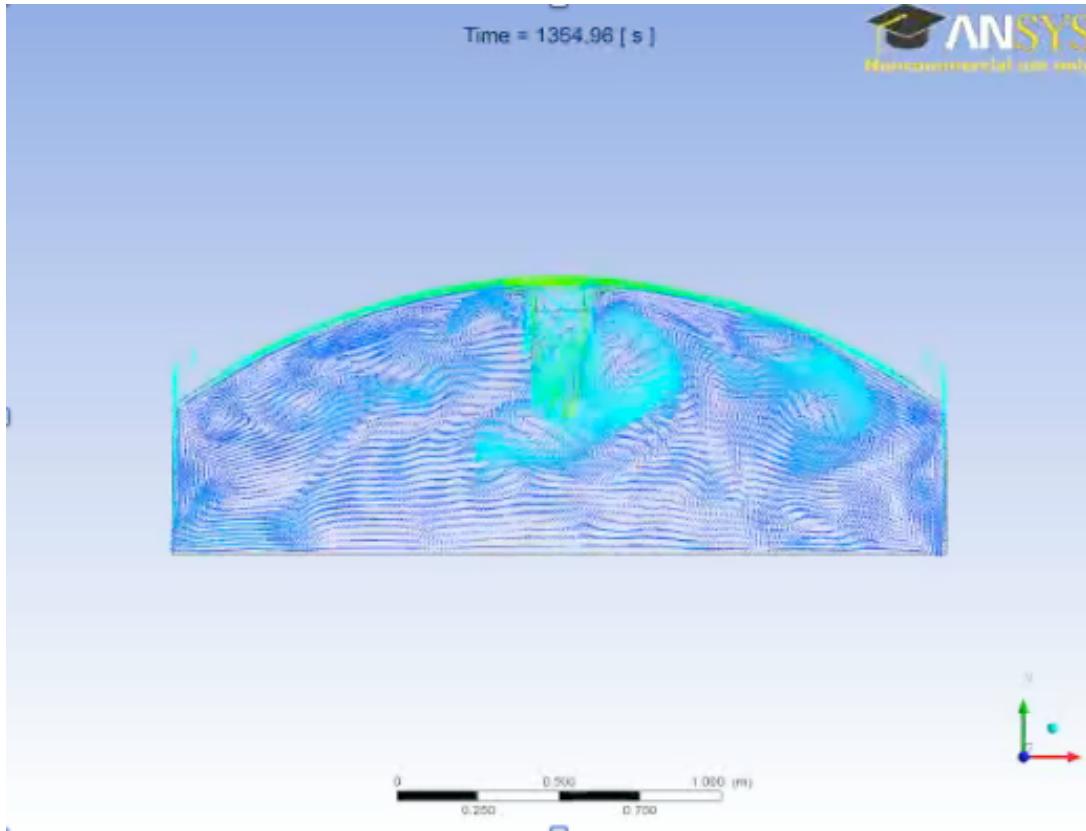
ANSYS Modeling - Convection

- Convection Modeling Constraints
 - Condenser Temp = 3.2 K
 - Fluid Temp = 4.2 K
 - Helium Vessel = Adiabatic or 4.3 K
 - Helium Gas (No condensation)
 - Total Time
 - Vessel Geometry
 - Condenser Geometry



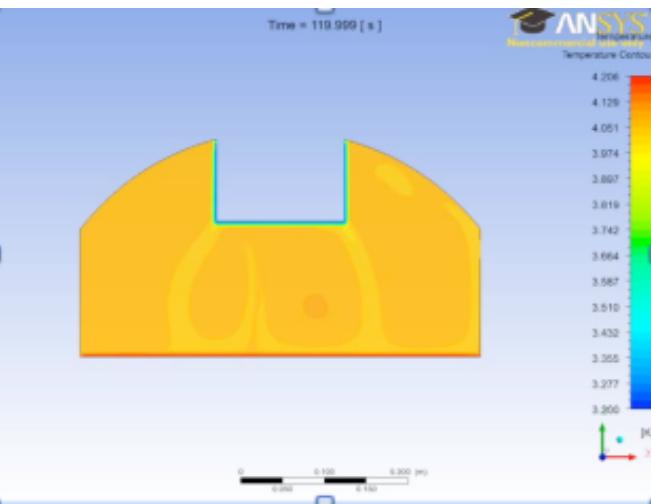
ANSYS Modeling - Convection

- Convection never reaches a steady state (long time runs)

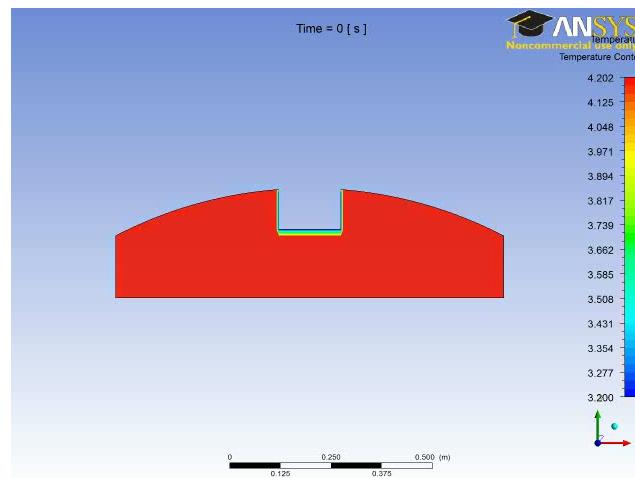


ANSYS Modeling - Convection (Increase Width)

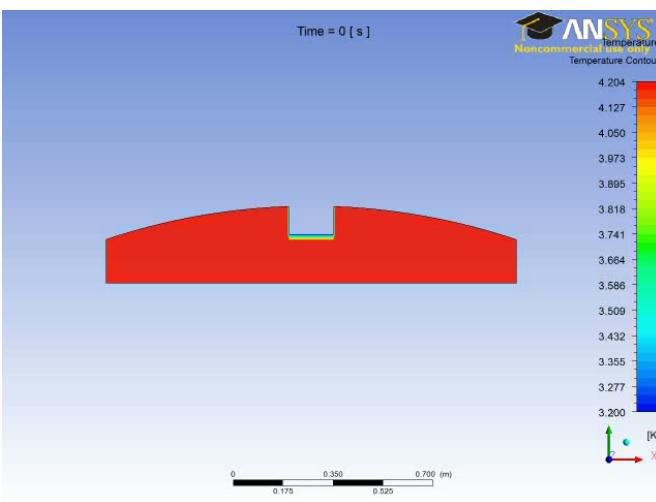
Conv22: H=1x, W=1x



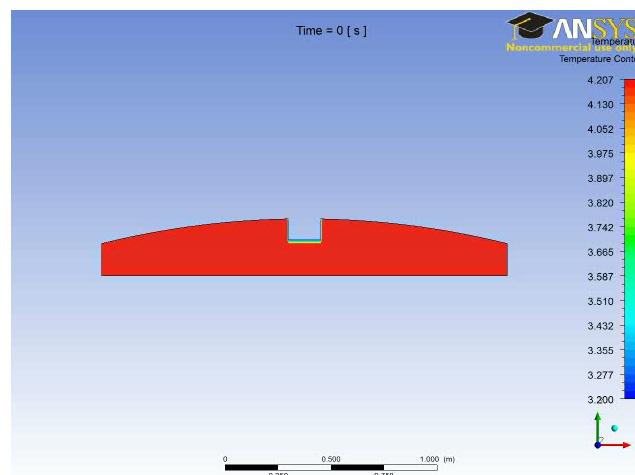
Conv20: H=1x, W=2x



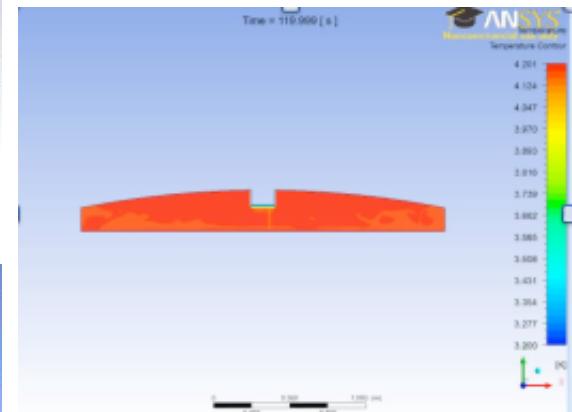
Conv21: H=1x, W=3x



Conv29: H=1x, W=4x

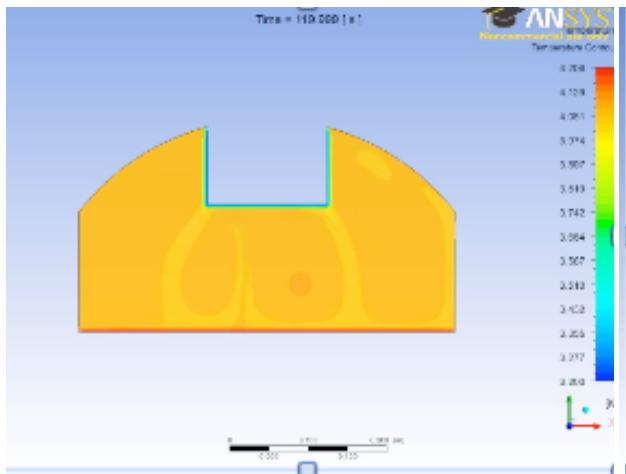


Conv23: H=1x, W=5x

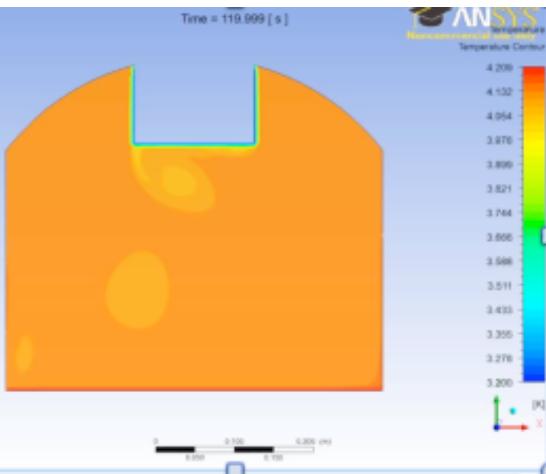


ANSYS Modeling - Convection (Increase height)

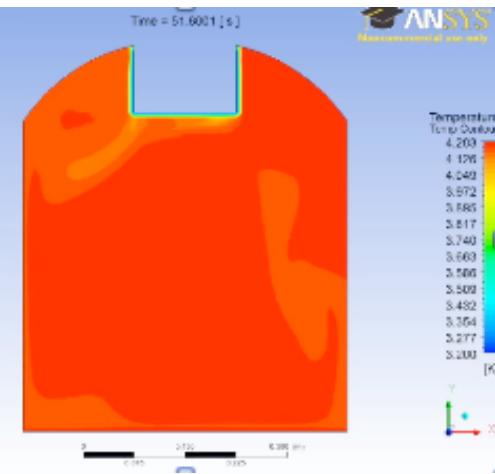
Conv22: H=1x, W=1x



Conv24: H=2x, W=1x

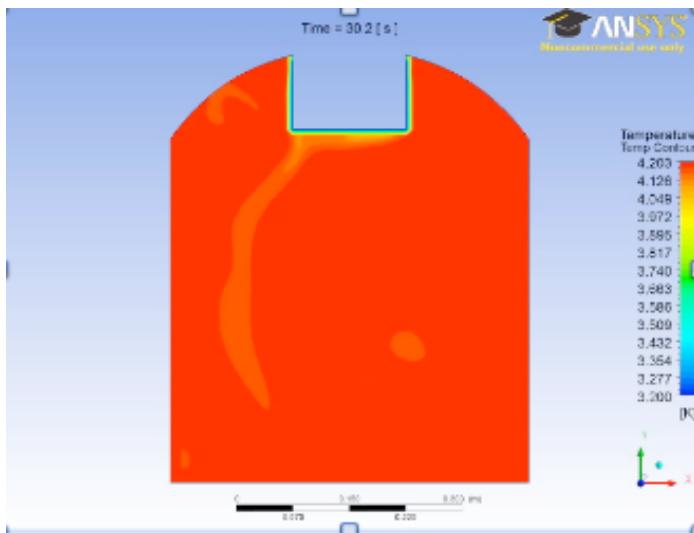


Conv7: H=3x, W=1x

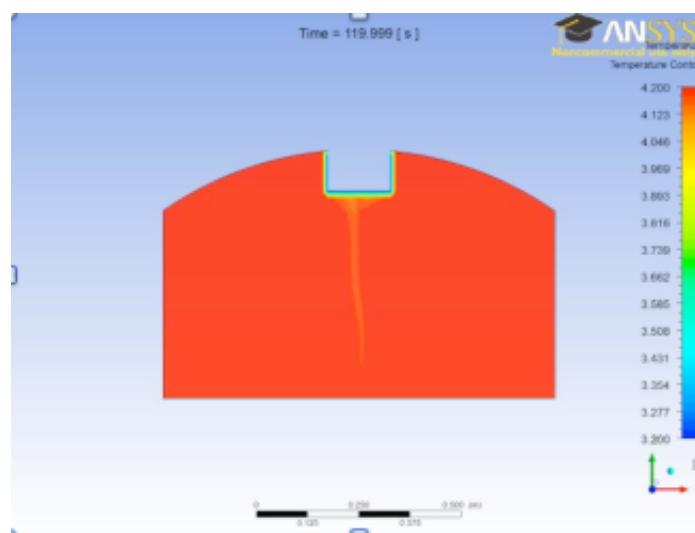


ANSYS Modeling - Convection (Very large vessels)

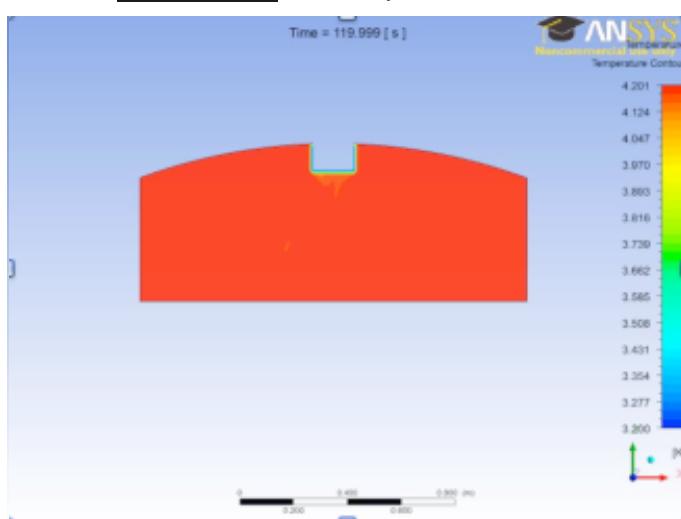
Conv7: H=3x, W=1x



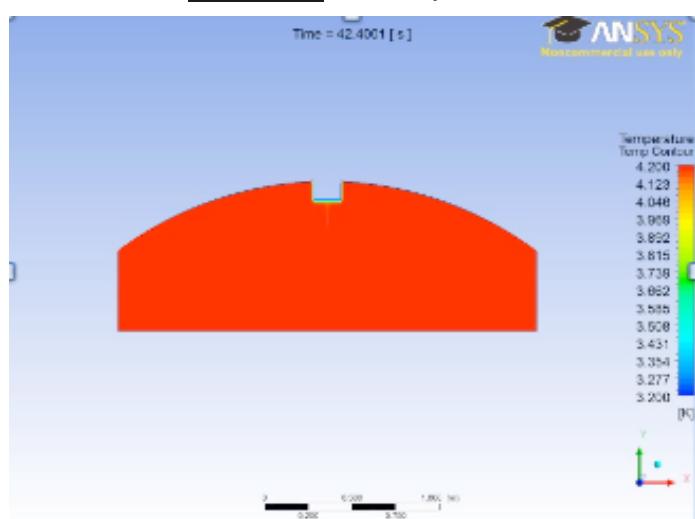
Conv17: H=3x, W=2x



Conv18: H=3x, W=3x

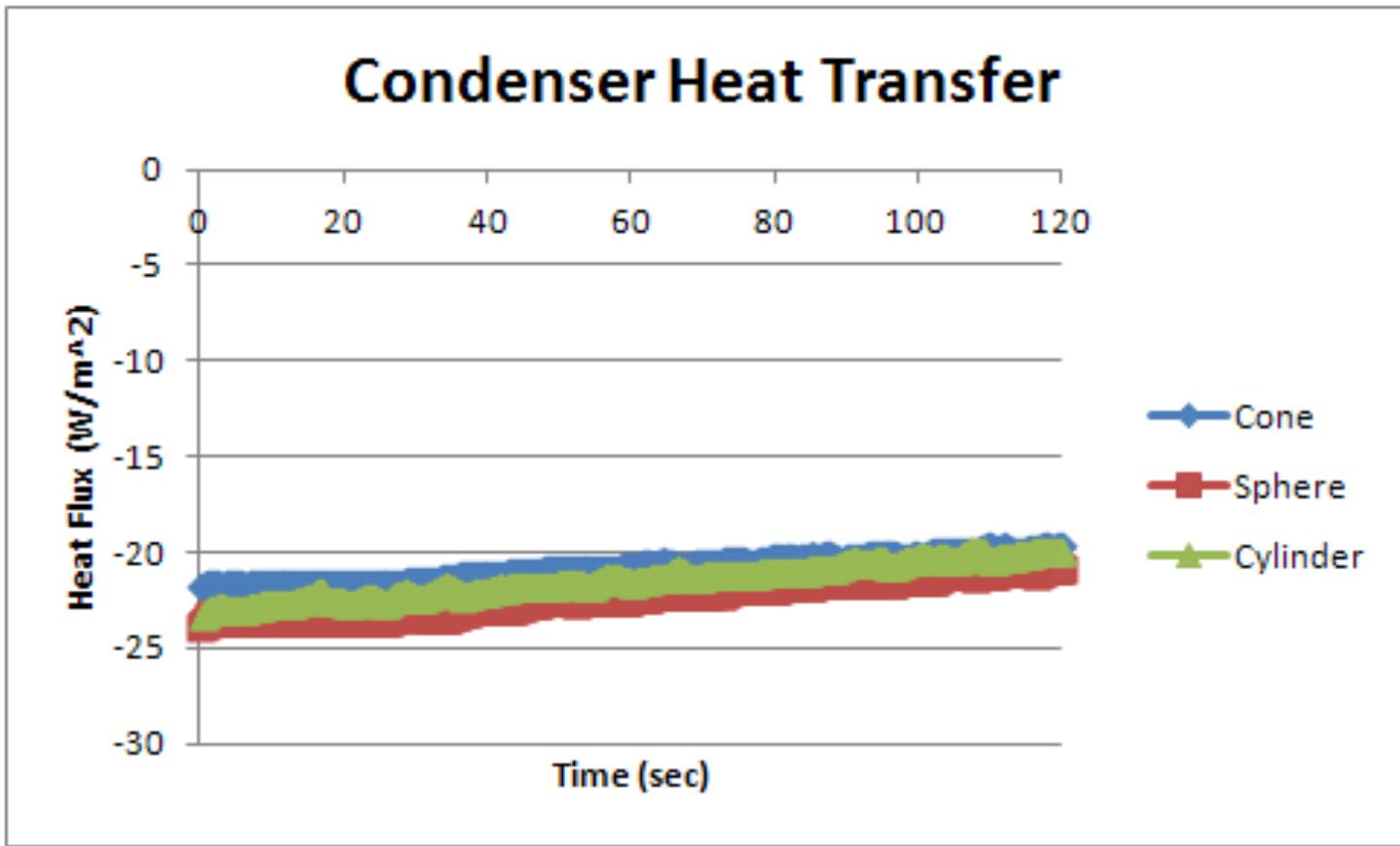


Conv8: H=3x, W=5x



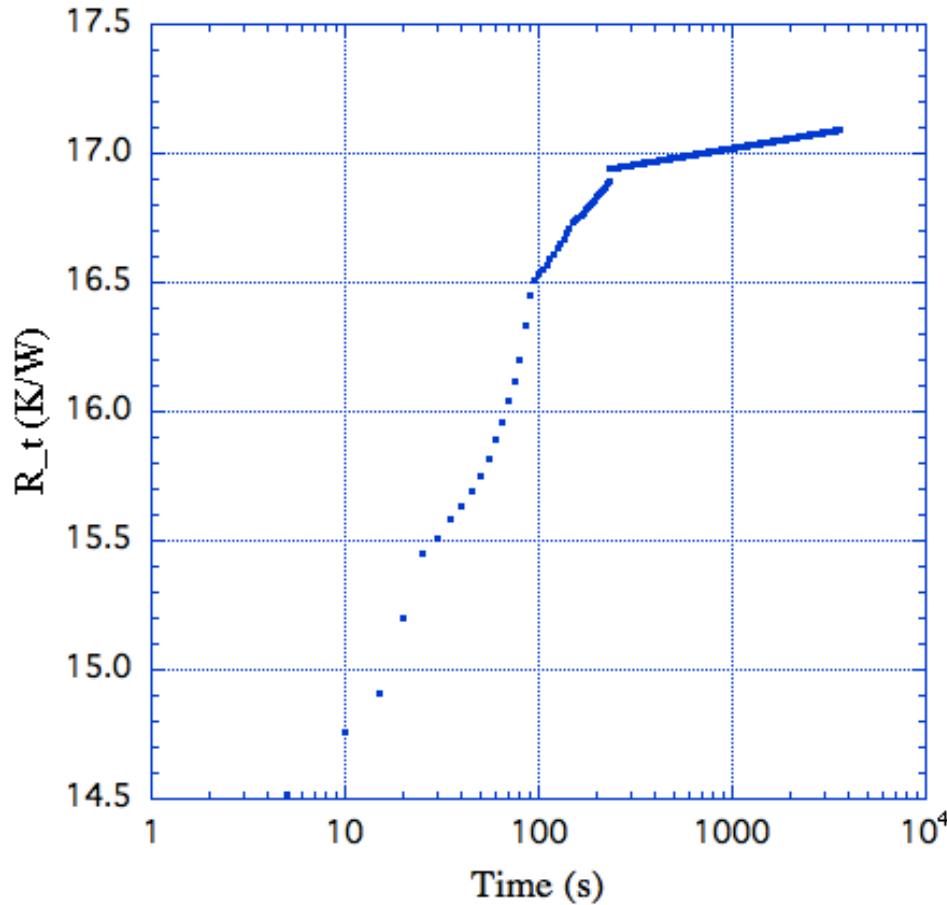
ANSYS Modeling - Convection

- Condensation tip geometry comparisons
- Little difference between condenser geometries



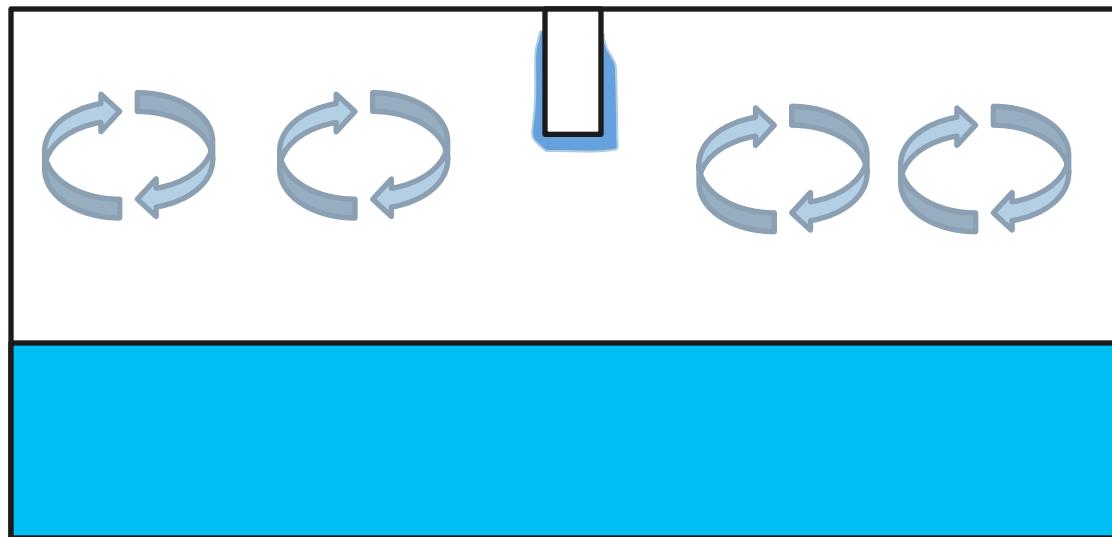
ANSYS Modeling - Convection

- Condensation tip geometry comparisons
- Little difference between condenser geometries



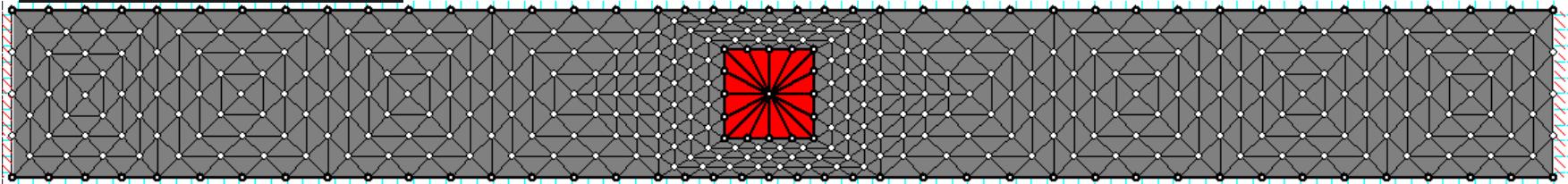
ANSYS Modeling (Convection) - Conclusions

- Size of the vessel impacts convection
- Geometry of condensation tip does not dramatically effect convection
- Order of magnitude for UW test quasi 'steady state' is 3-4 minutes
- Order of magnitude thermal resistance is 20 K/W

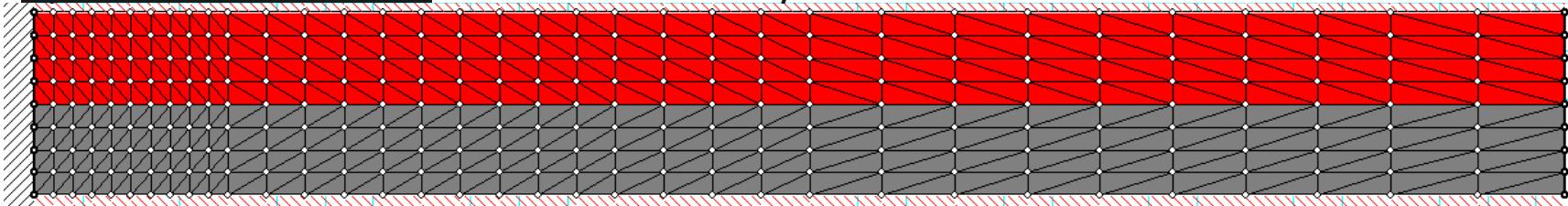


Thermal Resistance - Vessel Conduction (FEHT)

Cartesian Coordinates – Flatten vessel



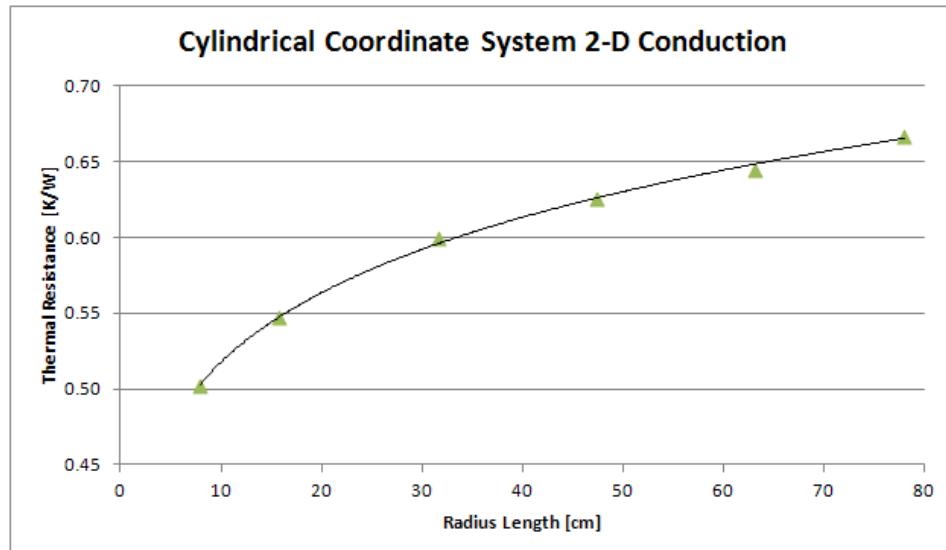
Cylindrical Coordinates – Rotate around cryocooler



- 3D to 2D approximation
- Weighted by cross-sectional area

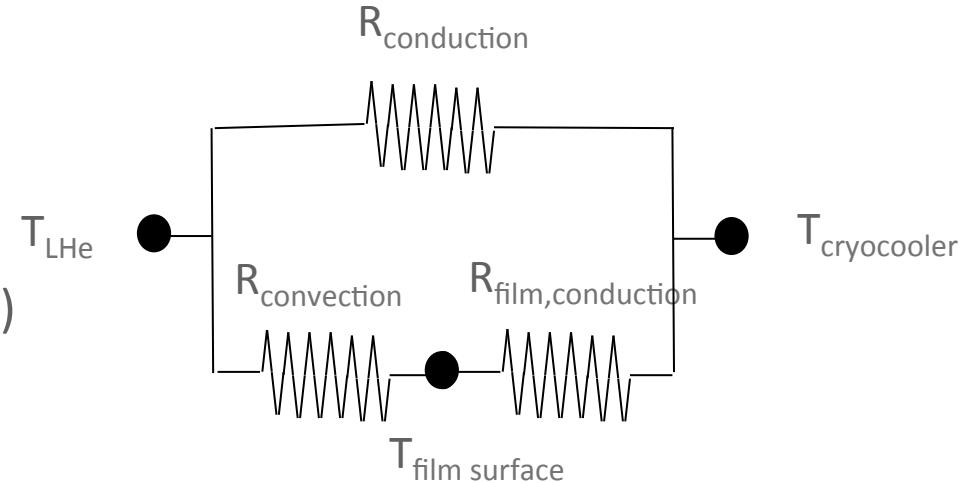
$$k_{eff}(4[K]) = \frac{A_{c,304SS}}{A_{ctot}} k_{304SS}(4[K]) + \frac{A_{c,Cu}}{A_{ctot}} k_{Cu}(4[K])$$

- Without copper
 - 3x higher thermal resistance



Modeling Conclusions

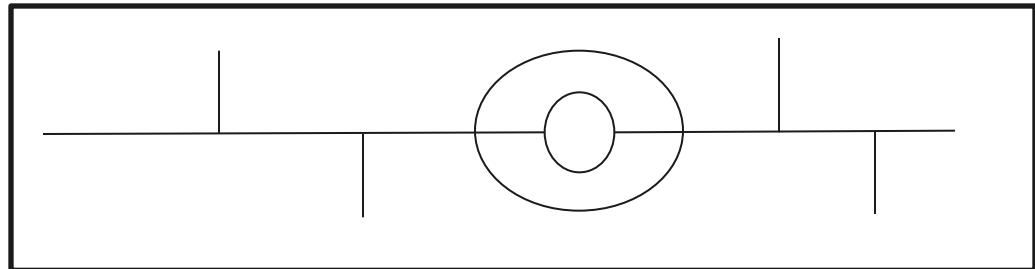
- Vessel conduction
 - $R_{\text{film,cond}} \approx 0.5 \text{ K/W}$
- Vapor convection
 - $R_{\text{conv}} \approx 20 \text{ K/W}$ (Dominant)
- Film condensation
 - $R_{\text{film,cond}} \approx 0.1 \text{ K/W}$



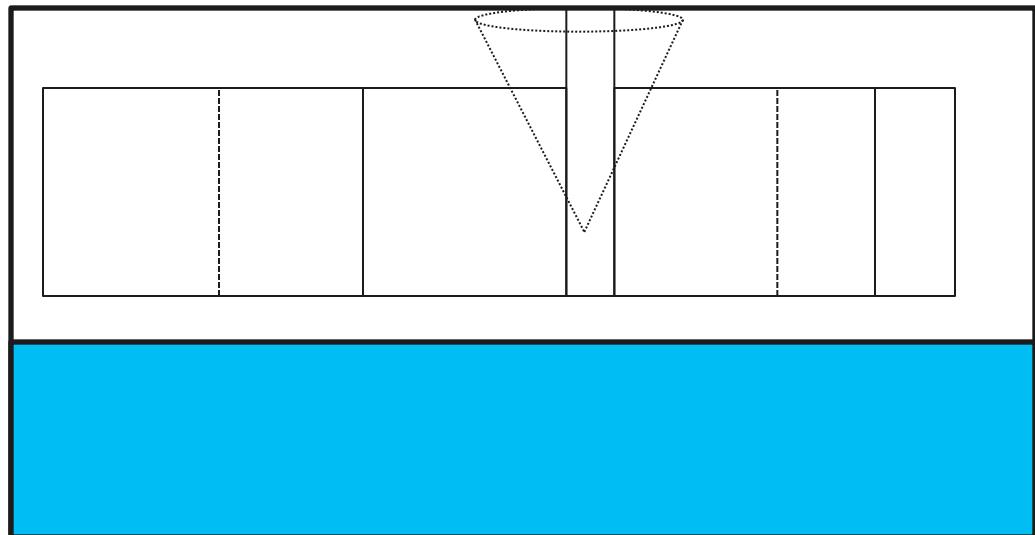
Extended Surfaces in Vapor Region

- Extended surface helps reduce convective thermal resistance
- Ideas
 - Copper sheets that fold open
 - Expandable aluminum foam

Top View

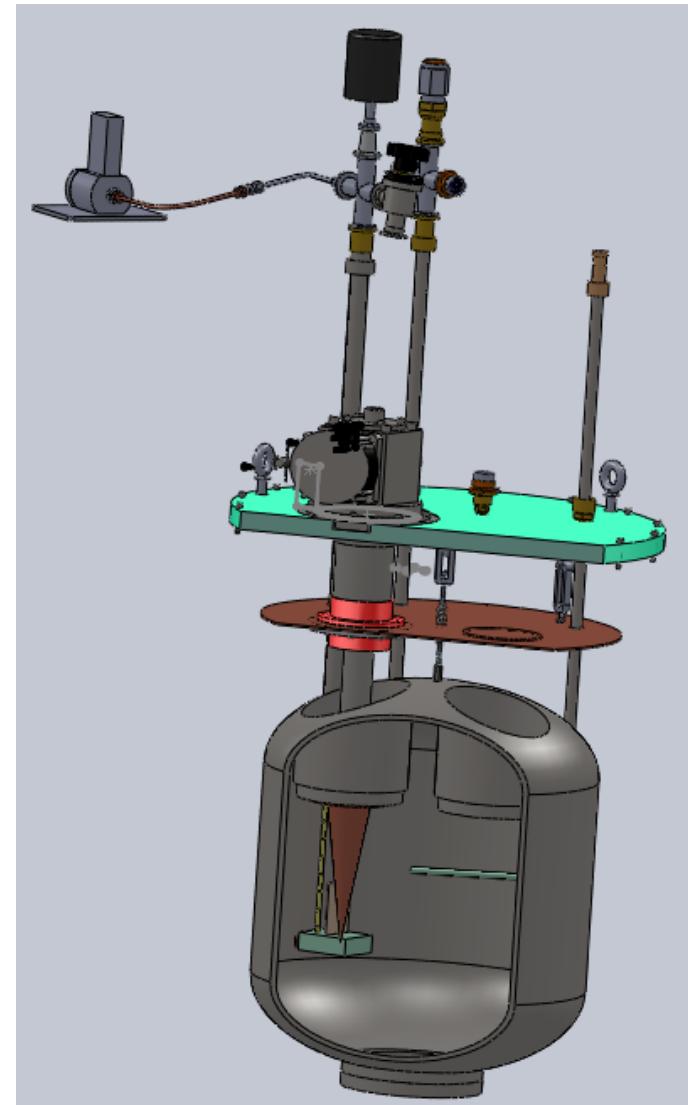
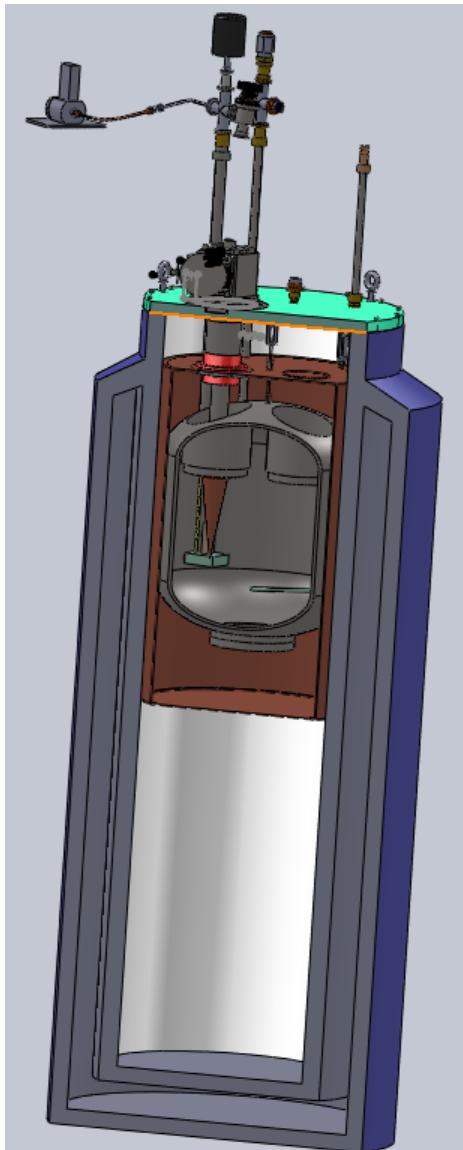


Side View



Experimental Work

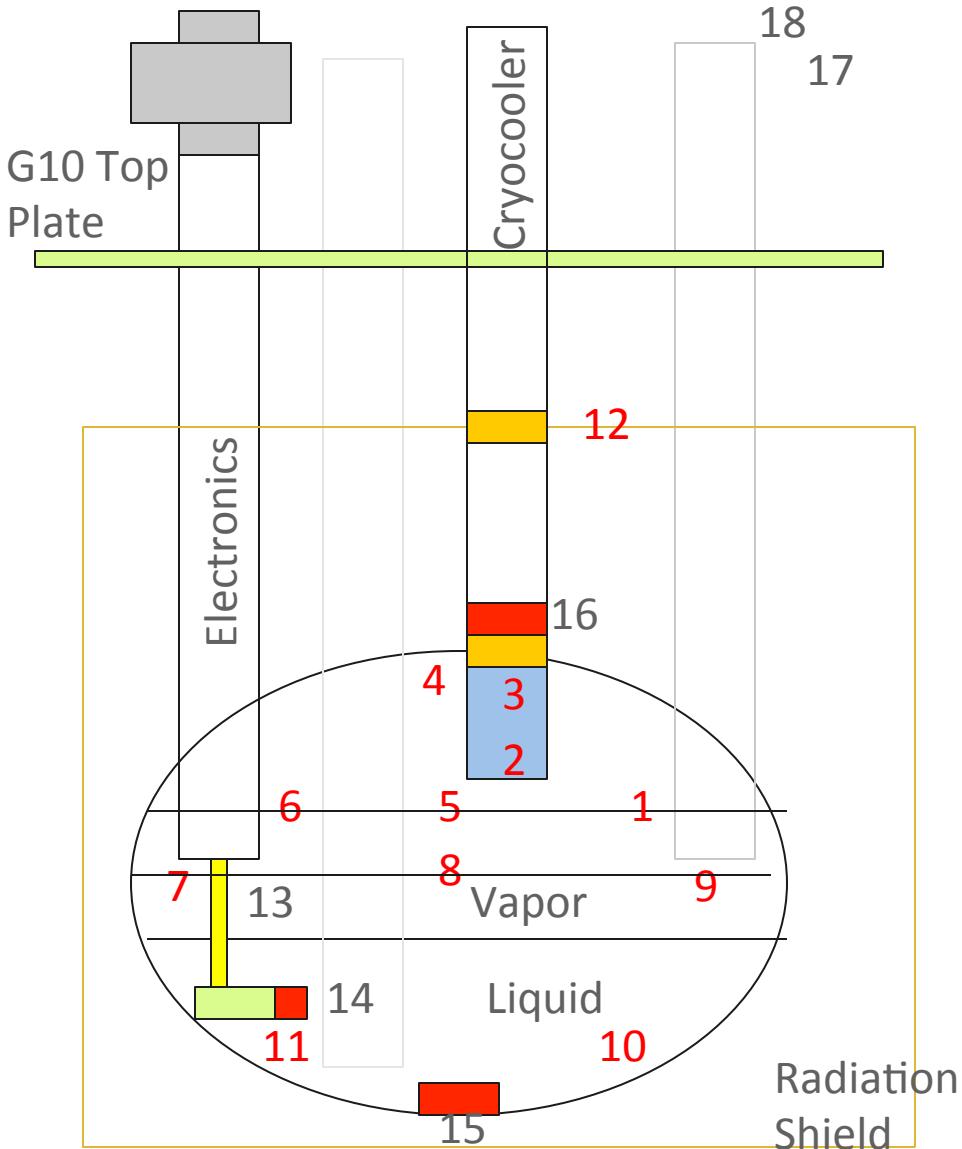
Experimental Setup - Cut Outs



Experimental Setup - Assembly & LN₂ Filling



Electronics Schematic



1-12. Thermometer (Cernox)

13. Liquid level indicator

14-16. Heater

17. Flow meter

18. Pressure transducer

- Characterize transient temperatures in the vapor region to compare to ANSYS modeling



Future Work

- Heat Transfer Flange Leak
 - Stainless Steel Backing Ring
- Run experiment
 - Baseline test (No cryocooler)
 - Bare cryocooler tip (with cryocooler)
 - Various extended surfaces
 - Surface enhancements

Acknowledgements

- Support from ANL
 - Elizabeth R. Moog, Yuri Ivanyushenkov, Joel Fuerst, Robert L Kustom, Quentin Hasse
- Work performed by Dan Schick
 - with assistance from Dan Potratz, Diego Fonseca, and others at UW-Madison

Questions?